



Gasification Research at OSU

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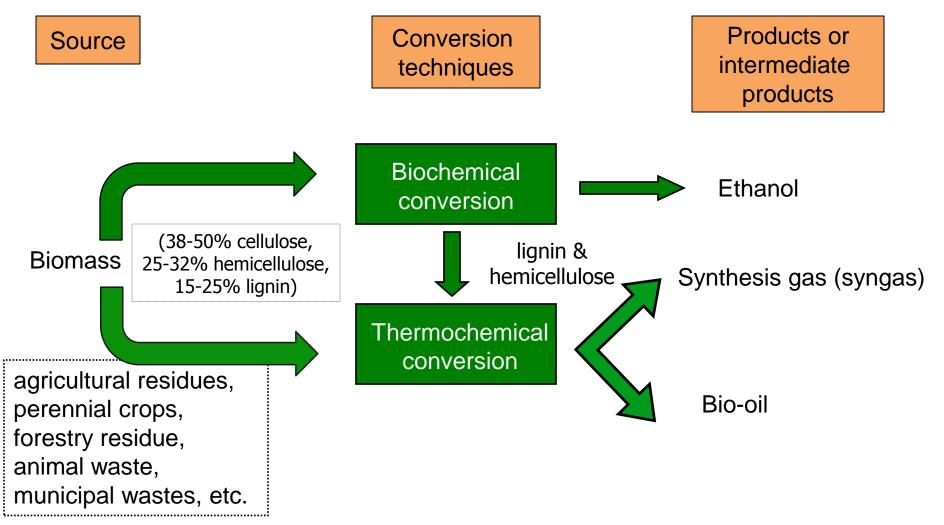
Biobased Products and Energy Center (BioPEC), Biosystems and Agricultural Engineering, Oklahoma State University

OK EPSCoR Annual State Conference





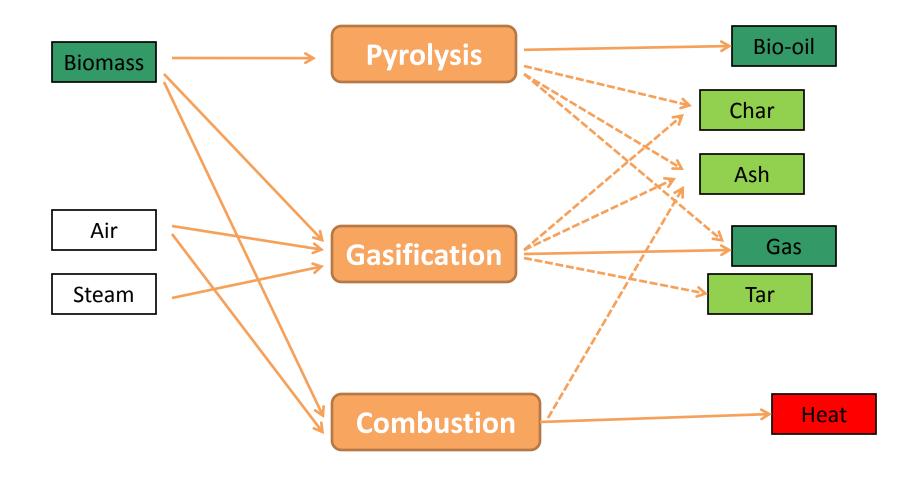
Energy conversion pathways







Thermochemical Conversions

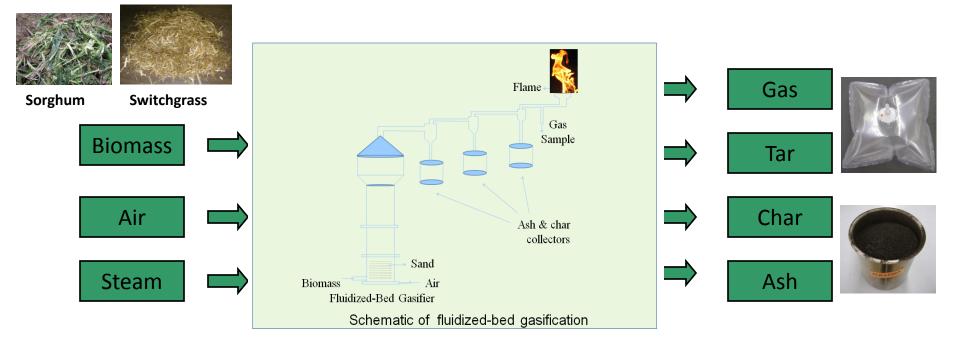


----->Byproduct



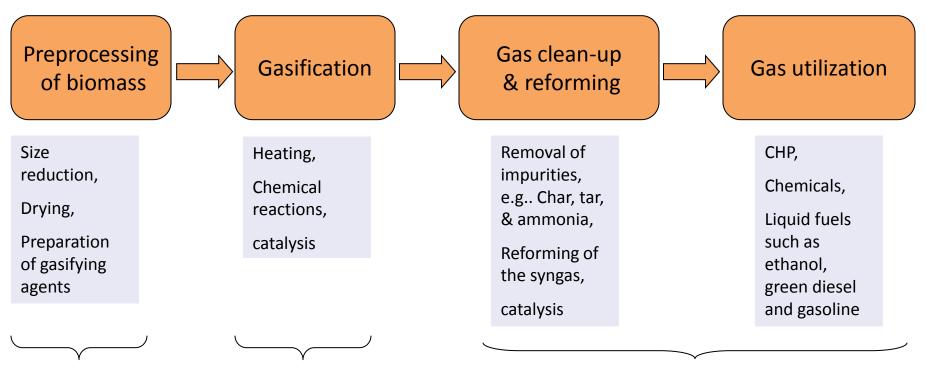


Gasification process



- Required: high temperature & oxidizing agent
- biomass + air + $H_2O \Rightarrow C$ (char)+ CH_4 + $CO + H_2 + + CO_2 + N_2 + H_2O$ (unreacted steam) + ash + tar



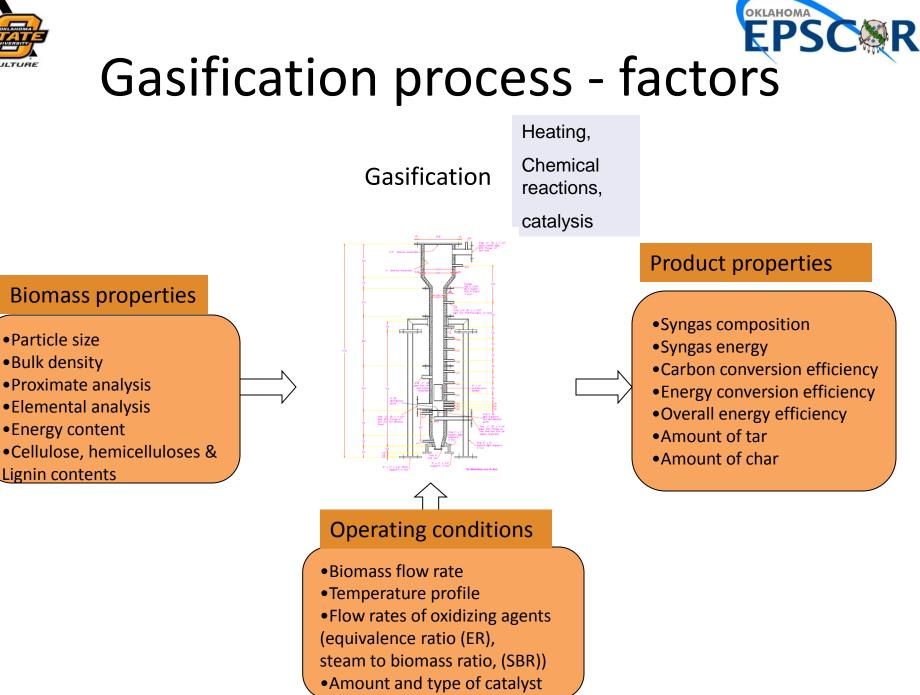


Upstream processing

Gasification

Downstream processing







- Experimental challenge
 - Understand and predict the effects of gasification conditions and biomass properties
 - Reduce level of tar and impurities in the producer gas
 - Optimize gasification operating conditions & gasifier design
 - Improve cold gas cleaning technique
 - Improve hot gas cleaning technique
 - Increase percentage compositions of CO and H₂
 - Increase net process energy efficiency
 - Obtain data for developing gasification reaction kinetics for a wide variety of feedstock
- Computational challenge
 - Develop gasification reaction kinetics
 - Incorporate reaction kinetics to develop gasification model to reliably predict gas composition, flowrate and contaminants





Ongoing Projects

- Study of fluidized-bed biomass gasification at near pilot-scale level.
- Study of downdraft biomass gasification at near pilot-scale level.
- Design and performance evaluation of a new lab-scale fluidizedbed gasifier.
- Evaluation of commercially-available catalysts for cracking tar and improving gas composition with toluene as a "model" tar compound.
- Design and development of catalytic reactor for cracking real tar and improving gas composition.
- Characterization of biomass for thermochemical conversion, and
- Development of reaction kinetics and mathematical model for predicting products of gasification



Study of FBG system at near pilot-scale



•Fluidized-bed Gasifier (FBG)



OKLAHOMA

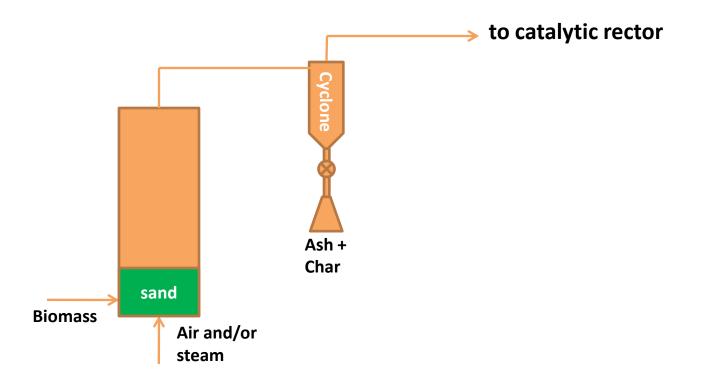
•Gas scrubbing system

•Biomass feedrate - 15-30 kg/h





Design and performance evaluation of new lab-scale FBG

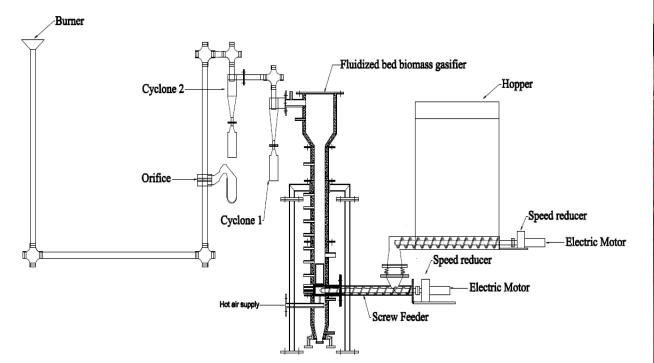


Objectives

- Design a new lab-scale FBG with many instrumentation and control
- Supply producer gas with tar to tar cracking catalytic reactor
- Utilize this FBG reactor serve as a platform for studying catalytic degradation of tar and effects of numerous variables



New lab-scale fluidized-bed EPSC R gasifier (FBG)



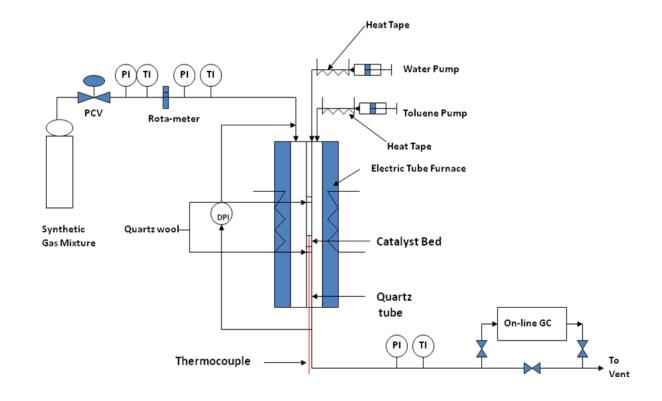


•Biomass feedrate – 3-5 kg/h





Evaluation of catalysts with toluene as a "model" tar compound



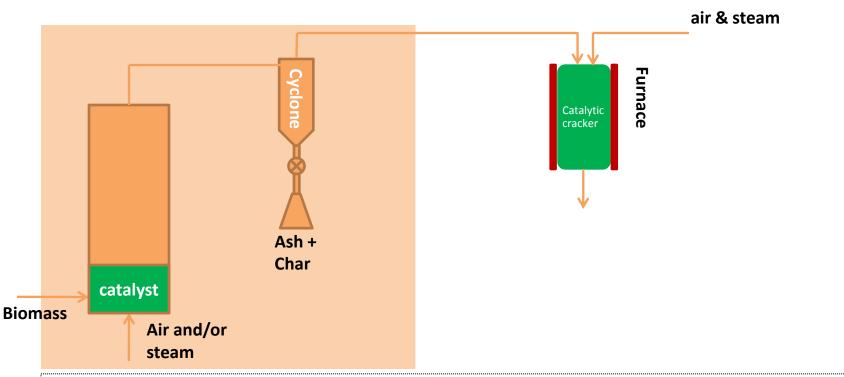
•Toluene is used as a model tar compound

•Tests are being conducted on selected steam reforming catalysts which are commercially available for cracking tar





Study of catalysts in a secondary reactor



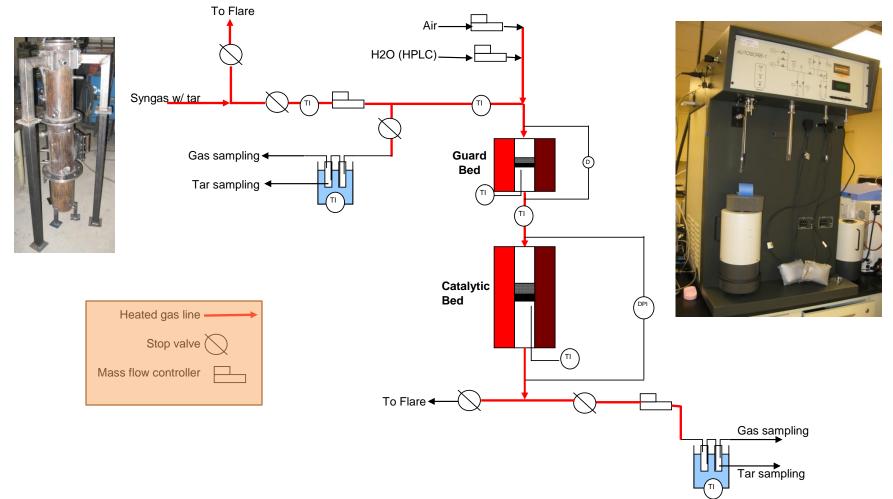
Objectives

- Study effects of operating condition of catalytic cracker (air and steam flowrate, temperature, residence time) and selected steam reforming catalysts for cracking tar and improving gas composition from gasifier.
- Field-test commercially-available catalysts





New catalytic Reactor for hot gas cleaning



Objectives

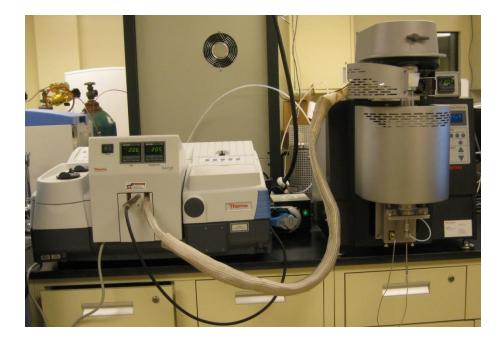
 Study effects of operating condition of catalytic cracker (air and steam flowrate, temperature, residence time) and various steam reforming catalysts on tar level and gas composition

Catalysts: commercial Ni-based steam reforming catalysts



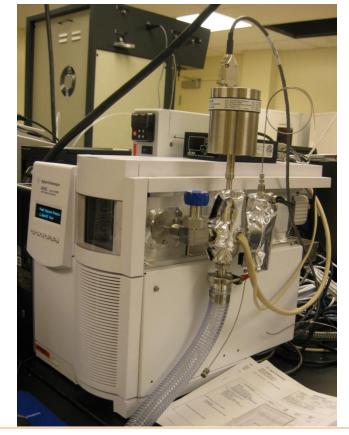


Biomass characterization for thermochemical conversion



Coupled TGA-FTIR set-up

Studying reaction kinetics of gasification
Identifying compounds at various reaction conditions

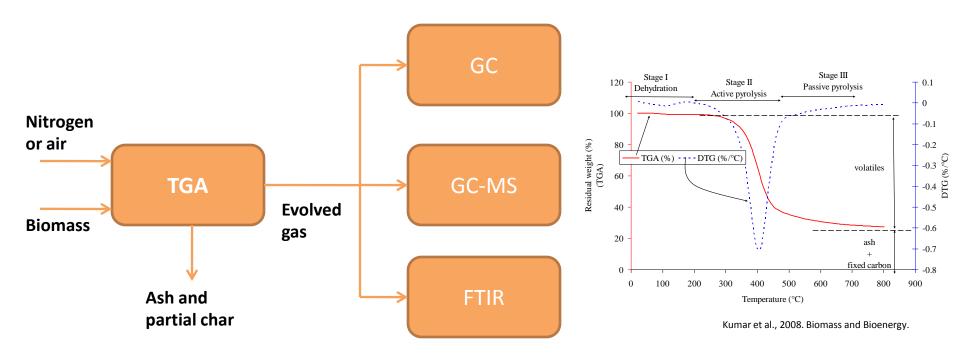


Mass Spec with precision sampling systemOnline measurement of gas composition





Reaction kinetics of gasification



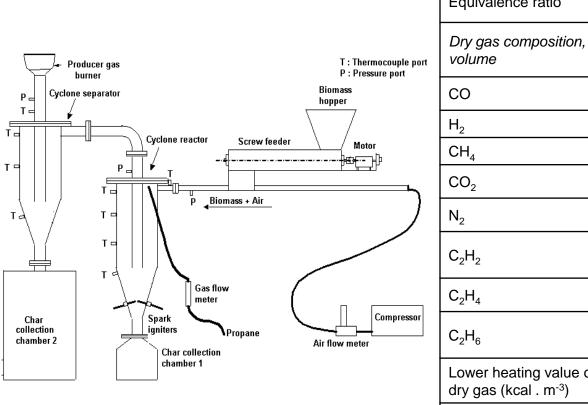
Objectives

- Investigate the effects of oxidizing atmosphere, temperature and heating rate on gas and tar composition
- Derive volatization kinetics of various feedstocks
- Develop gasification model to predict producer gas composition





Cyclone gasifier

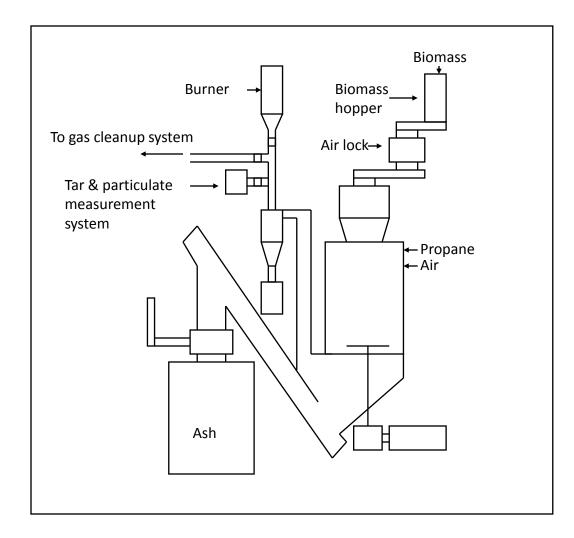


Equivalence ratio	0.12	0.15	0.15	0.15	0.22
Dry gas composition, % volume					
СО	17.5	15.7	19.7	19.9	20.2
H ₂	4.2	5.0	5.5	5.8	6.5
CH ₄	3.2	3.7	4.1	3.3	3.2
CO ₂	16.2	17.8	18.5	14.8	13.4
N ₂	57.9	55.3	49.5	53.7	55.0
C ₂ H ₂	Not detected	0.9	0.9	0.8	0.7
C ₂ H ₄	1.0	1.4	1.72	1.3	0.9
C ₂ H ₆	Not detected	0.2	0.2	0.4	0.2
Lower heating value of dry gas (kcal . m ⁻³)	1052	1273	1471	1395	1294
Dry gas yield (m ^{3 .} kg ⁻¹ dry biomass)	0.9	1.1	1.2	1.1	1.6
Char generation, % of fuel input	20	19	16	16	NA





Study on downdraft gasifier

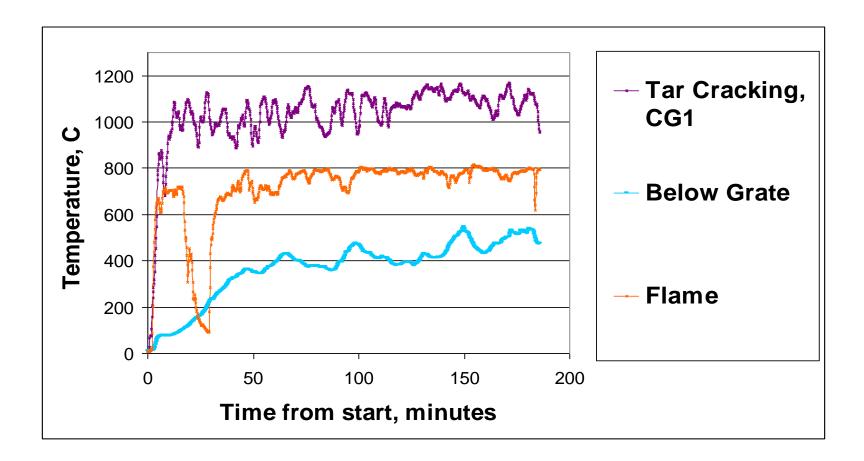






Temperature profile

for switchgrass gasification

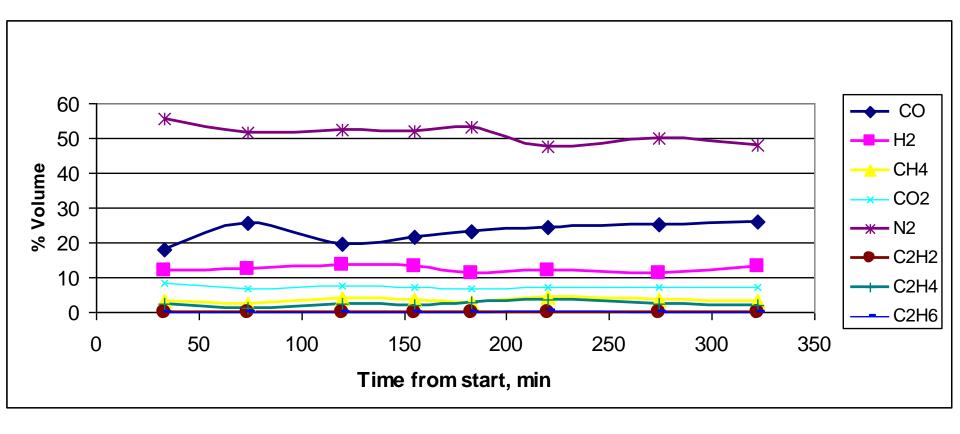






Gas composition

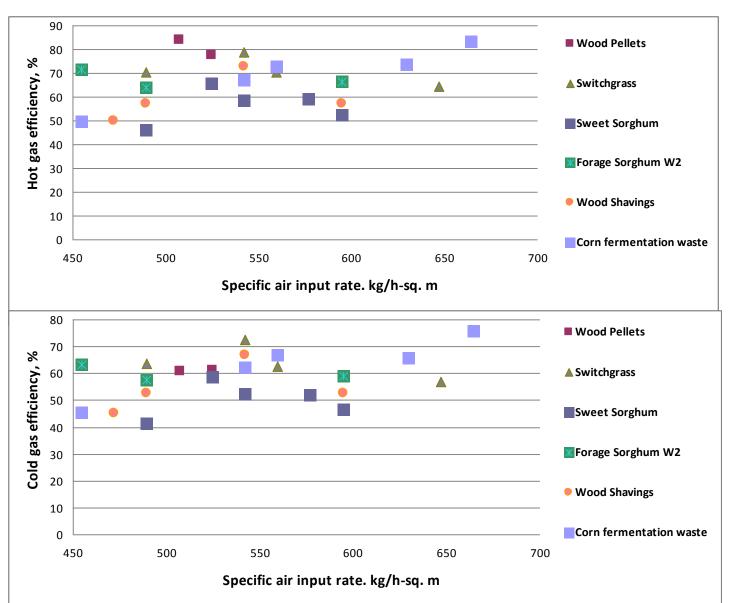
Switchgrass gasification





Energy Efficiency

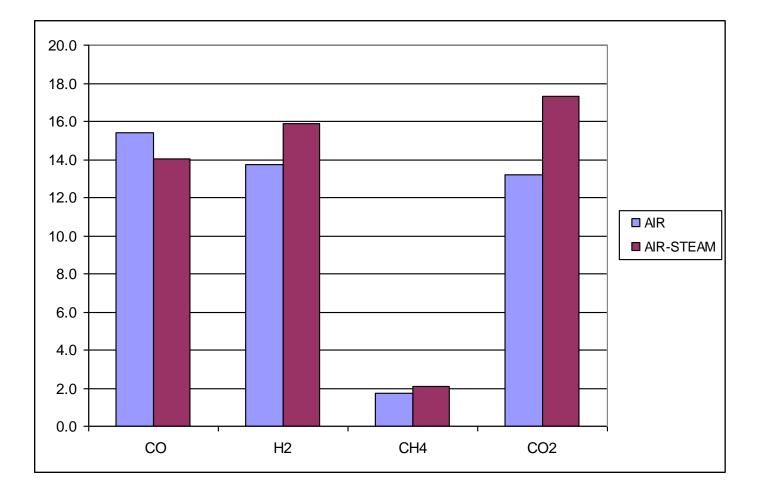








^{*}Air and air-steam gasification of chopped forage sorghum







Personnel and Financial Support

Pls:

- Ajay Kumar
- Krushna Patil
- Danielle Bellmer
- Raymond Huhnke

Graduate Students/Research engineer:

- Ashokkumar Sharma Design and study of lab-scale fluidized-bed gasification
- Prakash Bhoi Study of downdraft gasification
- Vamsee Pasangulapati Thermochemical characterization of biomass
- Sabre Arrowood Design and study of new catalytic tar cracker
- Akshata Modinoor Study on effects of catalytic reactor condition on tar cracking
- Luz Martin Evaluation of the selected catalysts for tar cracking
- Financial Support provided by:
 - Oklahoma State Regents for Higher Education
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 - Oklahoma Bioenergy Center
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 - Director of the Oklahoma Agricultural Experiment Station





Thank you,

Questions?